AMENDMENTS TO THE CLAIMS

IN THE CLAIMS:

- 1. (Currently Amended) An elimination process of fluorinated anionic <u>surfactants</u> sufactants from exhausted gaseous streams wherein the gaseous stream is put into contact with aqueous solutions having pH from 3.5 to 13.8, the aqueous solution density being lower than 1.05 g/cm³, preferably lower than 1.03 g/cm³, wherein the concentration in the aqueous solution of the fluorinated anionic surfactant removed from the gaseous stream is lower than or equal to 70 ppm; preferably lower than or equal to 60 ppm, still more preferably lower than 50 ppm.
- 2. (Currently Amended) A <u>The</u> process according to claim 1, wherein the anionic fluorinated surfactants are selected from perfluorinated carboxylic acids or derivatives thereof, preferably perfluoroctanoate in acid or salified form.
- (Currently Amended) A <u>The</u> process according to claim 1, wherein the contact between the gaseous stream and the aqueous solutions is carried out in a scrubber.
- 4. (Currently Amended) A <u>The</u> process according to claim 3, wherein the used absorption column scrubber is a filling up column, preferably structured, a plate column or a spray column; preferably a spray column is used.
- 5. (Currently Amended) A <u>The</u> process according to claim 1, wherein one the process operates in a discontinuous or a continuous way, preferably in a continuous way.

- 6. (Currently Amended) A <u>The process according to claim 5</u>, wherein one <u>the process</u> operates in <u>the [[a]] continuous way according to one of the following methods a method selected from the group consisting of:</u>
 - by recycling the solution and recovering the surfactant at each recycle[[,]];
 - by recycling the solution until reaching a surfactant concentration of 70 ppm and then by treating <u>a</u> [[the]] liquid phase to remove the surfactant[[,]];
 - by using in the gas absorption phase scrubber fresh solution without recycle[[,]]; and
 - by feeding a fresh aqueous solution aliquot and drawing from the plant scrubber an aliquot containing the anionic surfactants to be sent to a recovery plant recovered.
- 7. (Currently Amended) A <u>The</u> process according to claim 5, wherein when one <u>the</u> <u>process</u> operates in [[a]] <u>the</u> discontinuous way, the solution used in the absorption <u>column scrubber</u> is recycled until a surfactant concentration of 70 ppm is reached.
- 8. (Currently Amended) A <u>The</u> process according to claim 1, wherein the surfactant is recovered from the aqueous solution flowing out from the absorption column by ene of the following methods a method selected from the group consisting of:
 - by passing the solution on anionic exchange resins[[,]];
 - by using specific adsorbers for fluorinated surfactants[[,]]:
 - by reverse osmosis units[[,]]; and
 - by precipitation with polivalent cation salts.
- 9. (Currently Amended) A <u>The</u> process according to claim 8, wherein a strong anionic exchange resin is used.

- 10. (Currently Amended) A <u>The process according to claim 8</u>, wherein the used specific adsorbers are selected from <u>the group consisting of active carbon</u>, aluminas, <u>and silicas</u>.
- 11. (Currently Amended) A <u>The</u> process according to claim 1, wherein the initial removal solution, and/or the recycle solution have a temperature in the range 5°C-40°C preferably 10°C-30°C.
- 12. (Currently Amended) A <u>The</u> process according to claim 1, wherein, in the scrubber, the ratio by weight among the flow rates of the feeding aqueous solution and fed <u>feed</u> gas is from 2 to 20, preferably from 4 to 15.
- 13. (New) The process of claim 1, wherein the aqueous solution density is lower than 1.03 g/cm³.
- 14. (New) The process of claim 1, wherein the concentration in the aqueous solution of the fluorinated anionic surfactant removed from the gaseous stream is lower than or equal to 60 ppm.
- 15. (New) The process of claim 1, wherein the concentration in the aqueous solution of the fluorinated anionic surfactant removed from the gaseous stream is lower than 50 ppm.
- 16. (New) The process of claim 2, wherein the anionic fluorinated surfactants are perfluorooctanoate in acid or salified form.
- 17. (New) The process of claim 4, wherein the scrubber is one member selected from the group consisting of a structured column, a plate column and a spray column.
- 18. (New) The process of claim 4, wherein the scrubber is the structured column.

- 19. (New) The process of claim 11, wherein the temperature is in the range of 10°C-30°C.
- 20. (New) The process of claim 12, wherein the ratio is from 4 to 15.